

MODEL-FREE CONTROL AND INTELLIGENT PID CONTROLLERS: TOWARDS A POSSIBLE TRIVIALIZATION OF NONLINEAR CONTROL?

Michel FLIESS ^{*,**} Cédric JOIN ^{*,***}

^{*} *INRIA-ALIEN*

^{**} *LIX (CNRS, UMR 7161), École polytechnique
91128 Palaiseau, France*

Michel.Fliess@polytechnique.edu

^{***} *CRAN (CNRS, UMR 7039), Nancy-Université
BP 239, 54506 Vandœuvre-lès-Nancy, France
Cedric.Join@cran.uhp-nancy.fr*

Abstract. We are introducing a model-free control and a control with a restricted model for finite-dimensional complex systems. This control design may be viewed as a contribution to “intelligent” PID controllers, the tuning of which becomes quite straightforward, even with highly nonlinear and/or time-varying systems. Our main tool is a newly developed numerical differentiation. Differential algebra provides the theoretical framework. Our approach is validated by several numerical experiments.

1. INTRODUCTION

Writing down simple and reliable differential equations for describing a concrete plant is almost always a daunting task. How to take into account, for instance, frictions, heat effects, ageing processes, characteristics dispersions due to mass production, ...? Those severe difficulties explain to a large extent why the industrial world is not willing to employ most techniques stemming from “modern” control theory, which are too often based on a “precise” mathematical modeling, in spite of considerable advances during the last fifty years. We try here¹ to overcome this unfortunate

situation thanks to recent fast estimation methods.² Two cases are examined:

- (1) *Model-free control* is based on an elementary continuously updated *local* modeling via the unique knowledge of the input-output behavior. It should not be confused with the usual “black box” identification (see, *e.g.*, (Kersch, Worden, Vakakis & Golinval [2006], Sjöberg, Zhang, Ljung, Benveniste, Delyon, Glorennec, Hjalmarsson & Juditsky [1995])), where one is looking for a model which is valid within an operating range which should be as large as possible.³ Let us summarize our approach in the monovariate case. The

¹ This communication is a slightly modified and updated version of (Fliess & Join [2008a]), which is written in French. Model-free control and control with a restricted model, which might be useful for hybrid systems (Bourdais, Fliess, Join & Perruquetti [2007]), have already been applied in several concrete case-studies in various domains (Choi, d’Andréa-Novél, Fliess & Mounier [2009], Gédouin, Join, Delaleau, Bourgeot, Chirani & Calloch [2008], Join,

Masse & Fliess [2008], Villagra, d’Andréa-Novél, Fliess & Mounier [2008a,b]). Other applications on an industrial level are being developed.

² See, *e.g.*, (Fliess, Join & Sira-Ramírez [2008], Mboup, Join & Fliess [2009]) and the references therein.

³ This is why we use the terminology “model-free” and not “black box”.

input-output behavior of the system is assumed to “approximatively” governed within its operating range by an unknown finite-dimensional ordinary differential equation, which is not necessarily linear,

$$E(y, \dot{y}, \dots, y^{(a)}, u, \dot{u}, \dots, u^{(b)}) = 0 \quad (1)$$

We replace Eq. (1) by the following “phenomenological” model, which is only valid during a very short time interval,

$$y^{(\nu)} = F + \alpha u \quad (2)$$

The derivation order ν , which is in general equal to 1 or 2, and the constant parameter α are chosen by the practitioner. It implies that ν is not necessarily equal to the derivation order a of y in Eq. (1). The numerical value of F at any time instant is deduced from those of u and $y^{(\nu)}$, thanks to our numerical differentiators (Fliess, Join & Sira-Ramírez [2008], Mboup, Join & Fliess [2009]). The desired behavior is obtained by implementing, if, for instance, $\nu = 2$, the *intelligent PID controller*⁴ (*i-PID*)

$$u = -\frac{F}{\alpha} + \frac{\ddot{y}^*}{\alpha} + K_P e + K_I \int e + K_D \dot{e} \quad (3)$$

where

- y^* is the output reference trajectory, which is determined via the rules of flatness-based control (see, *e.g.*, Fliess, Lévine, Martin & Rouchon [1995], Rotella & Zambettakis [2007], Sira-Ramírez & Agrawal [2004]);
 - $e = y - y^*$ is the tracking error;
 - K_P, K_I, K_D are the usual tuning gains.
- (2) Assume now that a restricted or partial model of the plant is quite well known and is defined by Eq. (1) for instance. The plant is then governed by the *restricted*, or *incomplete*, modeling,⁵

$$E(y, \dot{y}, \dots, y^{(a)}, u, \dot{u}, \dots, u^{(b)}) + G = 0$$

where G stands for all the unknown parts.⁶ If the known system, which corresponds to $E = 0$, is flat, we also easily derive an *intelligent controller*, or *i-controller*, which gets rid of the unknown effects.

Differential algebra is briefly reviewed in Sect. 2 in order to

- derive the input-output differential equations,

- define minimum and non-minimum phase systems.

Numerical differentiation of noisy signals is examined in Sect. 3. Sect. 4 states the basic principles of our model-free control. Several numerical experiments⁷ are reported in Sect. 5. We deal as well with linear⁸ and nonlinear systems and with monovariable and multivariable systems. An anti-windup strategy is sketched in Sect. 5.4.2. Sect. 6 studies the control with a partially known modeling. One of the two examples deals with a non-minimum phase system.⁹ The numerical simulations of Sect. 5.1 and Sect. 6.2 show that our controllers behave much better than classic PIDs.¹⁰ Several concluding remarks are discussed in Sect. 7.

Remark 1. Only Sect. 2 is written in an abstract algebraic language. In order to understand the sequel and, in particular, the basic principles of our control strategy, it is only required to admit the input-output representations (1) and (4), as well as the foundations of flatness-based control (Fliess, Lévine, Martin & Rouchon [1995], Rotella & Zambettakis [2007], Sira-Ramírez & Agrawal [2004]).

2. NONLINEAR SYSTEMS

2.1 Differential fields

All the fields considered here are commutative and have characteristic 0. A *differential field*¹¹ \mathfrak{K} is a field which is equipped with a *derivation* $\frac{d}{dt}$, *i.e.*, a mapping $\mathfrak{K} \rightarrow \mathfrak{K}$ such that, $\forall a, b \in \mathfrak{K}$,

$$\bullet \frac{d}{dt}(a + b) = \dot{a} + \dot{b},$$

⁷ Those computer simulations would of course be impossible without precise mathematical models, which are *a priori* known.

⁸ The remark 9 underlines the following crucial fact: the usual mathematical criteria of robust control are becoming pointless in this new setting.

⁹ Non-minimum phase systems are today beyond our reach in the case of model-free control. This is certainly the most important theoretical question which is left open here.

¹⁰ We are perfectly aware that such a comparison might be objected. One could always argue that an existing control synthesis in the huge literature devoted to PIDs since Ziegler & Nichols [1942] (see, *e.g.*, Åström & Hägglund [2006], Åström & Murray [2008], Besançon-Voda & Gentil [1999], Dattaet, Ho & Bhattacharyya [2000], Dindeleux [1981], Franklin, Powell & Emami-Naeini [2002], Johnson & Moradi [2005], Lequesne [2006], O'Dwyer [2006], Rotella & Zambettakis [2008], Shinskey [1996], Visioli [2006], Wang, Ye, Cai & Hang [2008], Yu [1999]) has been ignored or poorly understood. Only time and the work of many practitioners will be able to confirm our viewpoint.

¹¹ See, *e.g.*, (Chambert-Loir [2005], Kolchin [1973]) for more details and, in particular, (Chambert-Loir [2005]) for basic properties of usual fields, *i.e.*, non-differential ones.

⁴ This terminology, but with other meanings, is not new in the literature (see, *e.g.*, Åström, Persson & Hang [1992]).

⁵ Since we are not employing the terminology “black box”, we are also here not employing the terminology “grey box”.

⁶ Any mathematical modeling in physics as well as in engineering is incomplete. Here the term G does not need to be “small” as in the classic approaches.

- $\frac{d}{dt}(ab) = \dot{a}b + a\dot{b}$.

A *constant* $c \in \mathfrak{K}$ is an element such that $\dot{c} = 0$. The set of all constant elements is the *subfield of constants*.

A differential field *extension* $\mathfrak{L}/\mathfrak{K}$ is defined by two differential fields $\mathfrak{K}, \mathfrak{L}$ such that:

- $\mathfrak{K} \subseteq \mathfrak{L}$,
- the derivation of \mathfrak{K} is the restriction to \mathfrak{K} of the derivation of \mathfrak{L} .

Write $\mathfrak{K}\langle S \rangle$, $S \subset \mathfrak{L}$, the differential subfield of \mathfrak{L} generated by \mathfrak{K} and S . Assume that $\mathfrak{L}/\mathfrak{K}$ is finitely generated, *i.e.*, $\mathfrak{L} = \mathfrak{K}\langle S \rangle$, where S est finite. An element $\xi \in \mathfrak{L}$ is said to be *differentially algebraic* over \mathfrak{K} if, and only if, it satisfies an algebraic differential equation $P(\xi, \dots, \xi^{(n)}) = 0$, where P is a polynomial function over \mathfrak{K} in $n+1$ variables. The extension $\mathfrak{L}/\mathfrak{K}$ is said to be *differentially algebraic* if, and only if, any element of \mathfrak{L} is differentially algebraic over \mathfrak{K} . The next result is important:

$\mathfrak{L}/\mathfrak{K}$ is differentially algebraic if, and only if, its transcendence degree is finite.

An element of \mathfrak{L} , which is non-differentially algebraic over \mathfrak{K} , is said to be *differentially transcendental* over \mathfrak{K} . An extension $\mathfrak{L}/\mathfrak{K}$, which is non-differentially algebraic, is said to be *differentially transcendental*. A set $\{\xi_i \in \mathfrak{L} \mid i \in I\}$ is said to be *differentially algebraically independent* over \mathfrak{K} if, and only if, there does not exists any non-trivial differential relation over \mathfrak{K} :

$Q(\dots, \xi_i^{(\nu_i)}, \dots) = 0$, where Q is a polynomial function over \mathfrak{K} , implies $Q \equiv 0$.

Two such sets, which are maximal with respect to set inclusion, have the same cardinality, *i.e.*, they have the same number of elements: this is the *differential transcendence degree* of the extension $\mathfrak{L}/\mathfrak{K}$. Such a set is a *differential transcendence basis*. It should be clear that $\mathfrak{L}/\mathfrak{K}$ is differentially algebraic if, and only if, its differential transcendence degree is 0.

2.2 Nonlinear systems

2.2.1. General definitions Let k be a given differential ground field. A *system*¹² is a finitely generated differentially transcendental extension \mathcal{K}/k . Let m be its differential transcendence degree. A set of (*independent*) *control variables* $\mathbf{u} = (u_1, \dots, u_m)$ is a differential transcendence basis of \mathcal{K}/k . The extension $\mathcal{K}/k\langle \mathbf{u} \rangle$ is therefore differentially algebraic. A set of *output variables* $\mathbf{y} = (y_1, \dots, y_p)$ is a subset of \mathcal{K} .

¹²See also (Delaleau [2002, 2008], Fliess, Join & Sira-Ramírez [2008], Fliess, Lévine, Martin & Rouchon [1995]) which provide more references on the use of differential algebra in control theory.

Let n be the transcendence degree of $\mathcal{K}/k\langle \mathbf{u} \rangle$ and let $\mathbf{x} = (x_1, \dots, x_n)$ be a transcendence basis of this extension. It yields the generalized state representation:

$$\begin{aligned} A_\iota(\dot{x}_\iota, \mathbf{x}, \mathbf{u}, \dots, \mathbf{u}^{(\alpha)}) &= 0 \\ B_\kappa(y_\kappa, \mathbf{x}, \mathbf{u}, \dots, \mathbf{u}^{(\beta)}) &= 0 \end{aligned}$$

where A_ι , $\iota = 1, \dots, n$, B_κ , $\kappa = 1, \dots, p$, are polynomial functions over k .

The following input-output representation is a consequence from the fact that y_1, \dots, y_p are differentially algebraic over $k\langle \mathbf{u} \rangle$:

$$\Phi_j(\mathbf{y}, \dots, \mathbf{y}^{(\bar{N}_j)}, \mathbf{u}, \dots, \mathbf{u}^{(\bar{M}_j)}) = 0 \quad (4)$$

where Φ_j , $j = 1, \dots, p$, is a polynomial function over k .

2.2.2. Input-output invertibility

- The system is said to be *left invertible* if, and only if, the extension¹³ $k\langle \mathbf{u}, \mathbf{y} \rangle / k\langle \mathbf{y} \rangle$ is differentially algebraic. It means that one can compute the input variables from the output variables via differential equations. Then $m \leq p$.
- It is said to be *right invertible* if, and only if, the differential transcendence degree of $k\langle \mathbf{y} \rangle / k$ is equal to p . This is equivalent saying that the output variables are differentially algebraically independent over k . Then $p \leq m$.

The system is said to be *square* if, and only if, $m = p$. Then left and right invertibilities coincide. If those properties hold true, the system is said to be *invertible*.

2.2.3. Minimum and non-minimum phase systems The ground field k is now the field \mathbb{R} of real numbers. Assume that our system is left invertible. The stable or unstable behavior of Eq. (4), when considered as a system of differential equations in the unknowns \mathbf{u} (\mathbf{y} is given) yields the definition of *minimum*, or *non-minimum*, *phase systems* (compare with Isidori [1999]).

3. NUMERICAL DIFFERENTIATION

The interested reader will find more details and references in (Fliess, Join & Sira-Ramírez [2008]). We refer to (Mboup, Join & Fliess [2009]) for crucial developments which play an important rôle in practical implementations.

¹³This extension $k\langle \mathbf{u}, \mathbf{y} \rangle / k\langle \mathbf{y} \rangle$ is called the *residual dynamics*, or the *zero dynamics* (compare with Isidori [1999]).

3.1 General principles

3.1.1. Polynomial signals Consider the polynomial time function of degree N

$$x_N(t) = \sum_{\nu=0}^N x^{(\nu)}(0) \frac{t^\nu}{\nu!}$$

where $t \geq 0$. Its operational, or Laplace, transform (see, e.g., Yosida [1984]) is

$$X_N(s) = \sum_{\nu=0}^N \frac{x^{(\nu)}(0)}{s^{\nu+1}} \quad (5)$$

Introduce $\frac{d}{ds}$, which is sometimes called the *algebraic derivation*. Multiply both sides of Eq. (5) by $\frac{d^\alpha}{ds^\alpha} s^{N+1}$, $\alpha = 0, 1, \dots, N$. The quantities $x^{(\nu)}(0)$, $\nu = 0, 1, \dots, N$, which satisfy a triangular system of linear equations, with non-zero diagonal elements,

$$\frac{d^\alpha s^{N+1} X_N}{ds^\alpha} = \frac{d^\alpha}{ds^\alpha} \left(\sum_{\nu=0}^N x^{(\nu)}(0) s^{N-\nu} \right) \quad (6)$$

are said to be *linearly identifiable* (Fliess & Sira-Ramírez [2003]). One gets rid of the time derivatives $s^\mu \frac{d^\mu X_N}{ds^\mu}$, $\mu = 1, \dots, N$, $0 \leq \iota \leq N$, by multiplying both sides of Eq. (6) by $s^{-\bar{N}}$, $\bar{N} > N$.

Remark 2. The correspondence between $\frac{d^\alpha}{ds^\alpha}$ and the product by $(-t)^\alpha$ (see, e.g., Yosida [1984]) permits to go back to the time domain.

3.1.2. Analytic signals A time signal is said to be *analytic* if, and only if, its Taylor expansion is convergent. Truncating this expansion permits to apply the previous calculations.

3.2 Noises

Noises are viewed here as quick fluctuations around 0. They are therefore attenuated by low-pass filters, like iterated integrals with respect to time.¹⁴

4. MODEL-FREE CONTROL: GENERAL PRINCIPLES

It is impossible of course to give here a complete description which would trivialize for practitioners the implementation of our control design. We hope that numerous concrete applications will make such an endeavor feasible in a near future.

4.1 Local modeling

- (1) Assume that the system is left invertible. If there are more output variables than input variable, i.e., $p \geq m$, pick up m output variables, say the first m ones, in order to get an invertible square system. Eq. (2) may be extended by writing

$$\begin{aligned} y_1^{(n_1)} &= F_1 + \alpha_{1,1}u_1 + \dots + \alpha_{1,m}u_m \\ &\dots \\ y_p^{(n_p)} &= F_m + \alpha_{m,1}u_1 + \dots + \alpha_{p,m}u_m \end{aligned} \quad (7)$$

where

- $n_j \geq 1$, $j = 1, \dots, p$, and, most often, $n_j = 1$ or 2 ;
 - $\alpha_{j,i} \in \mathbb{R}$, $i = 1, \dots, m$, $j = 1, \dots, p$, are *non-physical* constant parameters, which are chosen by the practitioner such that $\alpha_{j,i}u_i$ and F_j are of the same magnitude.
- (2) In order to avoid any algebraic loop, the numerical value of

$$F_j = y_j^{(n_j)} - \alpha_{j,1}u_1 - \dots - \alpha_{j,m}u_m$$

is given thanks to the time sampling

$$F_j(\kappa) = [y_j^{(n_j)}(\kappa)]_e - \sum_{i=1}^m \alpha_{j,i}u_i(\kappa - 1)$$

where $[\bullet(\kappa)]_e$ stands for the estimate at the time instant κ .

- (3) The determination of the reference trajectories for the output variables y_j is achieved in the same way as in flatness-based control.

Remark 3. It should also be pointed out that, in order to avoid algebraic loops, it is necessary that in Eq. (4)

$$\frac{\partial \Phi_j}{\partial y_j^{(n_j)}} \neq 0, \quad j = 1, \dots, p$$

It yields

$$n_j \leq \bar{N}_j$$

Numerical instabilities might appear when $\frac{\partial \Phi_j}{\partial y_j^{(n_j)}}$ is closed to 0.¹⁵

Remark 4. Our control design lead with non-minimum phase systems to divergent numerical values for the control variables u_j and therefore to the inapplicability of our techniques.

Remark 5. Remember that the Equations (1) and (4) are unknown. Verifying therefore the properties discussed in the two previous remarks may only be achieved experimentally within the plant operating range.

¹⁴See (Fliess [2006]) for a precise mathematical theory, which is based on *nonstandard analysis*.

¹⁵This kind of difficulties has not yet been encountered whether in the numerical simulations presented below nor in the quite concrete applications which were studied until now.

4.2 Controllers

Let us restrict ourselves for the sake of notations simplicity to monovariable systems.¹⁶ If $\nu = 2$ in Eq. (2), the intelligent PID controller has already been defined by Eq. (3). If $\nu = 1$ in Eq. (2), replace Eq. (3) by the *intelligent PI controller*, or *i-PI*,

$$u = -\frac{F}{\alpha} + \frac{\dot{y}^*}{\alpha} + K_P e + K_I \int e \quad (8)$$

Remark 6. Until now we were never obliged to chose $\nu \geq 2$ in Eq. (2). The previous controllers (3) and (8) might then be easily extended to the *generalized proportional integral controllers*, or *GPIs*, of (Fliess, Marquez, Delaleau & Sira-Ramírez [2002]).

Remark 7. In order to improve the performances it might be judicious to replace in Eq. (3) or in Eq. (8) the unique integral term $K_I \int e$ by a finite sum of iterated integrals

$$K_{I_1} \int e + K_{I_2} \int \int e + \dots + K_{I_\Lambda} \int \dots \int e$$

where

- $\int \dots \int e$ stands for the iterated integral of order Λ ,
- the K_{I_λ} , $\lambda = 1, \dots, \Lambda$, are gains.

We get if $K_{I_\Lambda} \neq 0$ an *intelligent $PI^\Lambda D$* or *PI^Λ* controller. Note also that setting $\Lambda = 0$ is a mathematical possibility. The lack of any integral term is nevertheless not recommended from a practical viewpoint.

Let us briefly compare our intelligent PID controllers to classic PID controllers:

- We do not need any identification procedure since the whole structural information is contained in the term F of Eq. (2), which is eliminated thanks to Eq. (3).
- The reference trajectories, which are chosen thanks to flatness-based methods, is much more flexible than the trajectories which are usually utilized in the industry. Overshoots and undershoots are therefore avoided to a large extent.

5. SOME EXAMPLES OF MODEL-FREE CONTROL

A zero-mean Gaussian white noise of variance 0.01 is added to all the computer simulations in order to test the robustness property of our control design. We utilize a standard low-pass filter with

classic controllers and the principles of Sect. 3.2 with our intelligent controllers.

5.1 A stable monovariable linear system

The transfer function

$$\frac{(s+2)^2}{(s+1)^3} \quad (9)$$

defines a stable monovariable linear system.

5.1.1. A classic PID controller We apply the well known method due to Broïda (see, *e.g.*, Dindeleux [1981]) by approximating the system (9) via the following delay system

$$\frac{Ke^{-\tau s}}{(Ts+1)}$$

$K = 4$, $T = 2.018$, $\tau = 0.2424$ are obtained thanks to graphical techniques. The gain of the PID controller are then deduced (Dindeleux [1981]): $K_P = \frac{100(0.4\tau+T)}{120K\tau} = 1.8181$, $K_I = \frac{1}{1.33K\tau} = 0.7754$, $K_D = \frac{0.35T}{K} = 0.1766$.

5.1.2. i-PI. We are employing $\dot{y} = F + u$ and the i-PI controller

$$u = -[F]_e + \dot{y}^* + PI(e)$$

where

- $[F]_e = [\dot{y}]_e - u$,
- y^* is a reference trajectory,
- $e = y - y^*$,
- $PI(e)$ is an usual PI controller.

5.1.3. Numerical simulations Fig. 1 shows that the i-PI controller behaves only slightly better than the classic PID controller. When taking into account on the other hand the ageing process and some fault accommodation there is a dramatic change of situation:

- Fig. 2 indicates a clear cut superiority of our i-PI controller if the ageing process corresponds to a shift of the pole from 1 to 1.5, and if the previous graphical identification is not repeated.
- The same conclusion holds, as seen Fig. 3, if there is a 50% power loss of the control.

Remark 8. This example shows that it might useless to introduce delay systems of the type

$$T(s)e^{-Ls}, \quad T \in \mathbb{R}(s), \quad L \geq 0 \quad (10)$$

for tuning classic PID controllers, as often done today in spite of the quite involved identification procedure. It might be reminded that

¹⁶The extension to the multivariable case is immediate. See Sect. 5.3.

- the structure and the control of systems of type (10) have been studied in (Fliess, Marquez & Mounier [2002]),
- their identification with techniques stemming also from (Fliess & Sira-Ramírez [2003]) has been studied in (Belkoura, Richard & Fliess [2009], Ollivier, Moutaouakil & Sadik [2007], Rudolph & Woittennek [2007]).

Remark 9. This example demonstrates also that the usual mathematical criteria for robust control become to a large irrelevant. Let us however point out that our control leads always to a pure integrator of order 1 or 2, for which the classic frequency techniques (see, *e.g.*, Åström & Murray [2008], Franklin, Powell & Emami-Naeini [2002], Rotella & Zambettakis [2008]) might still be of some interest.

Remark 10. As also shown by this example some fault accommodation may also be achieved without having recourse to a general theory of diagnosis.

5.2 A monovariable linear system with a large spectrum

With the system defined by the transfer function

$$\frac{s^5}{(s+1)(s+0.1)(s+0.01)(s-0.05)(s-0.5)(s-5)}$$

We utilize $\dot{y} = F + u$. A i-PI controller provides the stabilization around a reference trajectory. Fig. 4 exhibits an excellent tracking.

5.3 A multivariable linear system

Introduce the transfer matrix

$$\begin{pmatrix} \frac{s^3}{(s+0.01)(s+0.1)(s-1)s} & 0 \\ \frac{s+1}{(s+0.003)(s-0.03)(s+0.3)(s+3)} & \frac{s^2}{(s+0.004)(s+0.04)(s-0.4)(s+4)} \end{pmatrix}$$

For the corresponding system we utilize after a few attempts Eq. (7) with the following decoupled form

$$\dot{y}_1 = F_1 + 10u_1 \quad \dot{y}_2 = F_2 + 10u_2$$

The stabilization around a reference trajectory (y_1^*, y_2^*) is ensured by the multivariable i-PID controller

$$\begin{aligned} u_1 &= \frac{1}{10} \left(\dot{y}_1^* - F_1 + K_{P1}e_1 + K_{I1} \int e_1 + K_{D1}\dot{e}_1 \right) \\ u_2 &= \frac{1}{10} \left(\dot{y}_2^* - F_2 + K_{P2}e_2 + K_{I2} \int e_2 + K_{D2}\dot{e}_2 \right) \end{aligned}$$

where

- $e_1 = y_1^* - y_1$, $e_2 = y_2^* - y_2$;
- $K_{P1} = 1$, $K_{I1} = K_{D1} = 0$, $K_{P2} = K_{I2} = 50$, $K_{D2} = 10$.

The performances displayed on Fig. 5 and 6 are excellent. Fig. 6-(b) shows the result if we would set $F_1 = F_2 = 0$: it should be compared with Fig. 6-(a).

Remark 11. Model reduction is often utilized for the kind of systems studied in Sect. 5.2 and Sect. 5.3 (see, *e.g.*, Antoulas [2005], Obinata & Anderson [2001]).

5.4 An unstable monovariable nonlinear system

5.4.1. i-PID For $\dot{y} - y = u^3$ we utilize for Eq. (2) the local model $\dot{y} = F + u$. The stabilization around a reference trajectory y^* is provided by the i-PI controller

$$u = -F + \dot{y}^* + K_{PE} + K_I \int e \quad (11)$$

where $K_P = -2$, $K_I = -1$. The simulations displayed in Fig. 7 are excellent.

5.4.2. Anti-windup We now assume that u should satisfy the following constraints $-2 \leq u \leq 0.4$. The performances displayed by Fig. 8 are mediocre if an anti-windup is not added to the classic part of the i-PI controller. Our solution is elementary¹⁷: as soon as the control variable gets saturated, the integral $\int e$ in Eq. (11) is maintained constant.¹⁸

5.5 Ball and beam

Fig. 10 displays the famous ball and beam example, which obeys to the equation¹⁹ $\ddot{y} = By\dot{u}^2 - BG \sin u$, where $u = \theta$ is the control variable. This monovariable system, which is not linearizable by a static state feedback, is therefore not flat. It is thus difficult to handle.²⁰

We have chosen for Eq. (2) $\ddot{y} = F + 100u$. In order to satisfy as well as possible the experimental conditions, the control variable is saturated: $-\pi/3 < u < \pi/3$ and $-\pi < \dot{u} < \pi$. Fig. 11 and Fig. 12 display two types of trajectories: a Bézier polynomial and a sine function. We obtain in both cases excellent trackings thanks to an i-PID controller. In the Figures 11-(b), 12-(b), 11-(c), 12-(c) the control variable and the estimations of F

¹⁷ This is a well covered subject in the literature (see, *e.g.*, Bohn & Atherton [1995], Hippe [2006], Peng, Vrancic & Hanus [1996]).

¹⁸ Better performances would be easily reached, as flatness-based control is teaching us, with a modified reference trajectory.

¹⁹ The sine function which appears in that equation takes us outside of the theory sketched in Sect. 2. This difficulty may be easily circumvented by utilizing $\tan \frac{u}{2}$ (see Fliess, Lévine, Martin & Rouchon [1995]).

²⁰ A quite large literature has been devoted to this example (see, *e.g.*, (Fantoni & Lozano [2002], Hauser, Sastry & Kokotovic [1992], Sastry [1999]) for advanced nonlinear techniques, and (Zhang, Jiang & Wang [2002]) for neural networks). Let us add that all numerical simulations in those references are given without any corrupting noise.

are presented in the noiseless case. Compare with the Figures 11-(d) and 12-(d)) where a corrupting noise is added.

5.6 The three tank example

The three tank example in Fig. 13 is quite popular in diagnosis.²¹ It obeys to the equations:

$$\begin{cases} \dot{x}_1 = -C_1 \text{sign}(x_1 - x_3) \sqrt{|x_1 - x_3|} + u_1/S \\ \dot{x}_2 = C_3 \text{sign}(x_3 - x_2) \sqrt{|x_3 - x_2|} \\ \quad - C_2 \text{sign}(x_2) \sqrt{|x_2|} + u_2/S \\ \dot{x}_3 = C_1 \text{sign}(x_1 - x_3) \sqrt{|x_1 - x_3|} \\ \quad - C_3 \text{sign}(x_3 - x_2) \sqrt{|x_3 - x_2|} \\ y_1 = x_1 \\ y_2 = x_2 \\ y_3 = x_3 \end{cases}$$

where

$$\begin{aligned} C_n &= (1/S) \cdot \mu_n \cdot S_p \sqrt{2g}, n = 1, 2, 3; \\ S &= 0.0154 \text{ m (tank section);} \\ S_p &= 5.10^{-5} \text{ m (pipe section between the tanks);} \\ g &= 9.81 \text{ m.s}^{-2} \text{ (gravity);} \\ \mu_1 &= \mu_3 = 0.5, \mu_2 = 0.675 \text{ (viscosity coefficients).} \end{aligned}$$

As often in industry we utilize a zero-hold control (see Fig. 14-(c)). A decoupled Eq. (7) is employed here as we already did in Sect. 5.3: $\dot{y}_i = F_i + 200u_i, i = 1, 2$. Fig. 14-(a) displays the trajectories tracking. The derivatives estimation in Fig. 14-(b) is excellent in spite of the additive corrupting noise. The nominal controls (Fig. 14-(c)) are not very far from those we would have computed with a flatness-based viewpoint (see Fliess, Join & Sira-Ramírez [2005]). We also utilize the following i-PI controllers

$$u_i = \frac{1}{200} \left(\dot{y}_i^* - F_i + 10e_i + 2.10^{-2} \int e_i \right) \quad i = 1, 2$$

where y_i^* is the reference trajectory, $e_i = y_i^* - y_i$. In order to get a good estimate of e_i we are denoising y_i (see Fig. 14-(d)) according to the techniques of Sect. 3.

6. CONTROL WITH A RESTRICTED MODEL

6.1 General principles

6.1.1. Flatness The system (4) is assumed to be square, *i.e.*, $m = p$, and flat. Moreover $\mathbf{y} =$

(y_1, \dots, y_m) is assumed to be a flat output, *i.e.*, $\bar{M}_j = 0, j = 1, \dots, m$. It yields locally

$$u_j = \Psi_j(\mathbf{y}, \dots, \mathbf{y}^{(\bar{N}_j)}), \quad j = 1, \dots, m \quad (12)$$

Flatness-based control permits to select easily an efficient reference trajectory \mathbf{y}^* to which corresponds via Eq. (4) and Eq. (12) the open loop control \mathbf{u}^* . Let $\mathbf{e} = \mathbf{y} - \mathbf{y}^*$ be the tracking error. We assume the existence of a feedback controller $\mathbf{u}_{\text{feedback}}(\mathbf{e})$ such that

$$\mathbf{u} = \mathbf{u}^* + \mathbf{u}_{\text{feedback}}(\mathbf{e}) \quad (13)$$

ensures a stable tracking around the reference trajectory.

6.1.2. Intelligent controllers Replace Eq. (4) by

$$\Phi_j(\mathbf{y}, \dots, \mathbf{y}^{(\bar{N}_j)}, \mathbf{u}, \dots, \mathbf{u}^{(\bar{M}_j)}) + G_j = 0 \quad (14)$$

where the $G_j, j = 1, \dots, m$, stand for the unmodeled parts. Eq. (12) becomes then

$$u_j = \Psi_j(\mathbf{y}, \dots, \mathbf{y}^{(\bar{N}_j)}) + H_j, \quad j = 1, \dots, m \quad (15)$$

where $H_j \neq G_j$ in general. Thanks to Eq. (15), H_j is estimated in the same way as the fault variables and the unknown perturbations are in (Fliess, Join & Sira-Ramírez [2008]). Consider again \mathbf{y}^* and \mathbf{u}^* as they are defined above. The *intelligent controller*, or *i-controller*, follows from Eq. (13)

$$\mathbf{u} = \mathbf{u}^* + \begin{pmatrix} H_1 \\ \vdots \\ H_m \end{pmatrix} + \mathbf{u}_{\text{feedback}}(\mathbf{e})$$

It ensures tracking stabilization around the reference trajectory.

6.2 Frictions and nonlinearities

A point mass m at the end of a spring of length y obeys to the equation

$$m\ddot{y} = -\mathcal{K}(y) + \mathcal{F}(\dot{y}) - d\dot{y} + F_{\text{ext}} \quad (16)$$

where

- $F_{\text{ext}} = u$ is the control variable;
- d and $\mathcal{F}(\dot{y})$ are due to complex friction phenomena;
- $\mathcal{K}(y) = k_1 y + k_3 y^3$ exhibits a cubic nonlinearity of Duffing type;

The mass $m = 0.5$ is known; there is a possible error of 33% for $k_1 = 3$ and we utilize $\hat{k}_1 = 2$; d and k_3 , which are unknown, are equal to 5 and 10 in the numerical simulations. For the frictions,²²

²¹ See (Fliess, Join & Sira-Ramírez [2005]) for details and references. This paper was presenting apparently for the first time the diagnosis, the control and the fault accommodation of a nonlinear system with uncertain parameters. See also Fliess, Join & Sira-Ramírez [2008].

²² There is a huge literature in tribology where various possible friction models are suggested (see, *e.g.*, in control (Olsson, Åström, Canudas de Wit, Gäfvert & Lischinsky [1998], Nuninger, Perruquetti & Richard [2006]). Those modelings are bypassed here.

we have chosen for the sake of computer simulations the well known model due to Tustin [1947]. Fig. 15-(a) exhibits its quite wild behavior when the sign of the speed is changing.

6.2.1. A classic PID controller The PID controller is tuned only thanks to the restricted model $m\ddot{y} = -\hat{k}_1 y + u$. Its gains are determined in such a way that all the poles of the closed-loop system are equal to -3 : $K_P = -\hat{k}_1 + 27m$, $K_I = -27m$, $K_D = 9m$.

6.2.2. The corresponding i-PID controller Pick up a reference trajectory y^* . Set

$$u^* = m\ddot{y}^* + \hat{k}_1 y^*$$

Our i-PID controller is given by

$$F_{\text{ext}} = u = u^* - [\mathcal{G}]_e + \text{PID}(e) \quad (17)$$

where

- $\mathcal{G} = \mathcal{F}(\dot{y}) - (k_1 - \hat{k}_1)y - k_3 y^3 - d\dot{y}$, which stands for the whole set of unknown effects, is estimated via

$$[\mathcal{G}]_e = m[\ddot{y}]_e + \hat{k}_1[y]_e - F_{\text{ext}}$$

which follows from Eq. (16) ($[y]_e$ and $[\dot{y}]_e$ are the denoised output variable and its denoised 2nd-order derivative – see Fig. 15-(d,f));

- $\text{PID}(e)$, $e = y - y^*$, is the above classic PID controller.

6.2.3. Numerical simulations The performances of our i-PID controller (17), which are displayed in Fig. 15-(c,d), are excellent. When compared to the Figures

- 15-(e,f), where
 - flatness-based control is employed for determined the open-loop output and input variables,
 - the loop is closed via a classic PID controller, which does not take into account the unknown effects;
- 15-(g,h), where only a classic PID controller is used, without any flatness-based control;

the superiority of our control design is obvious. This superiority is increasing with the friction.

6.3 Non-minimum phase systems

Consider the transfer function

$$\frac{s - a}{s^2 - (b + c)s + bc}$$

$a, b, c \in \mathbb{R}$ are respectively its zero and its two poles. The corresponding input-output system is

non-minimum phase if $a > 0$. The controllable and observable state-variable representation

$$\begin{cases} \dot{x}_1 = x_2 \\ \dot{x}_2 = (b + c)x_2 - bcx_1 + u \\ y = x_2 - ax_1 \end{cases} \quad (18)$$

shows that $z = x_1$ is a flat output. The flat output is therefore not the measured output, as we assumed in Sect. 6.1.1. Our control design has therefore to be modified.

6.3.1. Control of the exact model To a nominal flat output²³ z^* corresponds a nominal control variable

$$u^* = \ddot{z}^* - (b + c)\dot{z}^* + bcz^*$$

and a nominal output variable

$$y^* = \dot{z}^* - az^* \quad (19)$$

Introduce the *GPI* controller (Fliess, Marquez, Delaleau & Sira-Ramírez [2002])

$$u = u^* + \gamma \int (u - u^*) + K_P(y - y^*) + K_I \int (y - y^*) + K_{II} \iint (y - y^*) \quad (20)$$

where the coefficients $\gamma, K_P, K_I, K_{II} \in \mathbb{R}$ are chosen in order to stabilize the error dynamics $e = z - z^*$. Excellent performances are displayed in Figures 16-(a) and (b), where $a = 1$, $b = -1$, $c = -0.5$, even with an additive corrupting noise. See Figures 16-(c) and (d) for y^* and z^* which is calculated by integrating Eq. (19) back in time.

6.3.2. Unmodeled effects The second line of Eq. (18) may be written again as

$$\dot{x}_2 = (b + c)x_2 - bcx_1 + u + \varpi$$

where ϖ stands for the unmodeled effects, like frictions or an actuator's fault. Replace the nominal control variable u^* of Sect. 6.3.1 by

$$u_{\text{pert}}^* = u^* - [\varpi]_e$$

where $[\varpi]_e$ is the estimated value of ϖ , which is given by

$$[\varpi]_e = - \left(\frac{[\ddot{y}]_e - (b + c)[\dot{y}]_e + bc[y]_e - [\dot{u}]_e}{a} + u \right)$$

Moreover,

$$[\dot{u}]_e = \dot{u}^* + \gamma(u - u^*) + K_P([\dot{y}]_e - \dot{y}^*) + K_I([y]_e - y^*) + K_{II} \int ([y]_e - y^*)$$

follows from Eq. (20).

Start with the Figures 17 and 18, where $\varpi = -0.5$, $a = 1$, $b = -1$, $c = -0.5$. Fig. 17-(b), where the nominal control is left unmodified, and Fig. 17-(e), where it is modified, demonstrate a clear-cut

²³ This Section, which is based on previous studies (Fliess & Marquez [2000], Fliess, Marquez, Delaleau & Sira-Ramírez [2002]), should make the reading of Sect. 6.3.2 easier.

superiority of our approach, even with an additive corrupting noise.

In Fig. 19, ϖ is no more assumed to be constant, but equal to $-0.1\dot{y}$. In the numerical simulations, $a = 2$, $b = -1$, $c = 1$. If ϖ is not estimated, it influences the tracking quite a lot even if its amplitude is weak. When ϖ is estimated on the other hand, the results are excellent, even with an additive corrupting noise.

7. CONCLUSION

The results which were already obtained with our intelligent PID controllers lead us to the hope that they will greatly improve the practical applicability and the performances of the classic PIDs, at least for all finite-dimensional systems which are known to be non-minimum phase within their operating range:

- the tuning of the gains of i-PIDs is straightforward since
 - the unknown part is eliminated,
 - the control design boils down to a pure integrator of order 1 or 2;
- the identification techniques for implementing classic PID regulators, which are often imprecise and difficult to handle, are becoming obsolete.

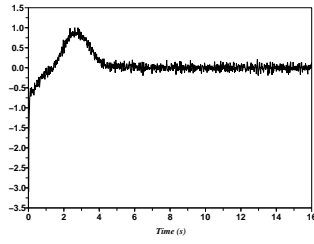
Model-free control and the control with a restricted model seem to question the very principles of modeling in applied sciences, at least when one wishes to control some concrete plant. This might be a fundamental “epistemological” change, which needs of course to be further discussed and analyzed. A natural extension to uncontrolled systems is being developed via various questions in financial engineering: see already the preliminary studies in (Fliess & Join [2008b, 2009a,b]).

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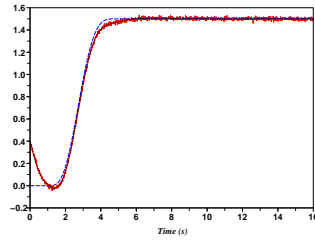
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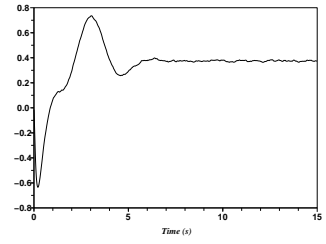
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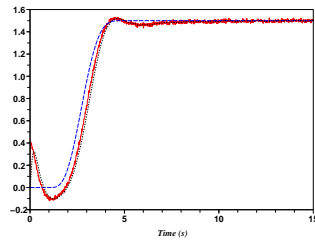
(a) i-PI control



(b) Output (-); reference (- -); denoised output (. .)

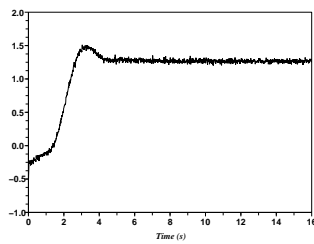


(c) PID control

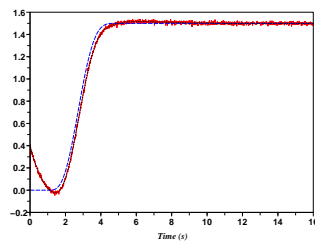


(d) Output (-); reference (- -); denoised output (. .)

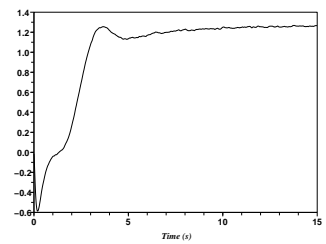
Figure 1. Stable linear monovariabile system



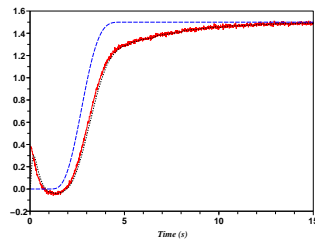
(a) i-PI control



(b) Output (-); reference (- -); denoised output (. .)



(c) PID control



(d) Output (-); reference (- -); denoised output (. .)

Figure 2. Modified stable linear monovariabile system

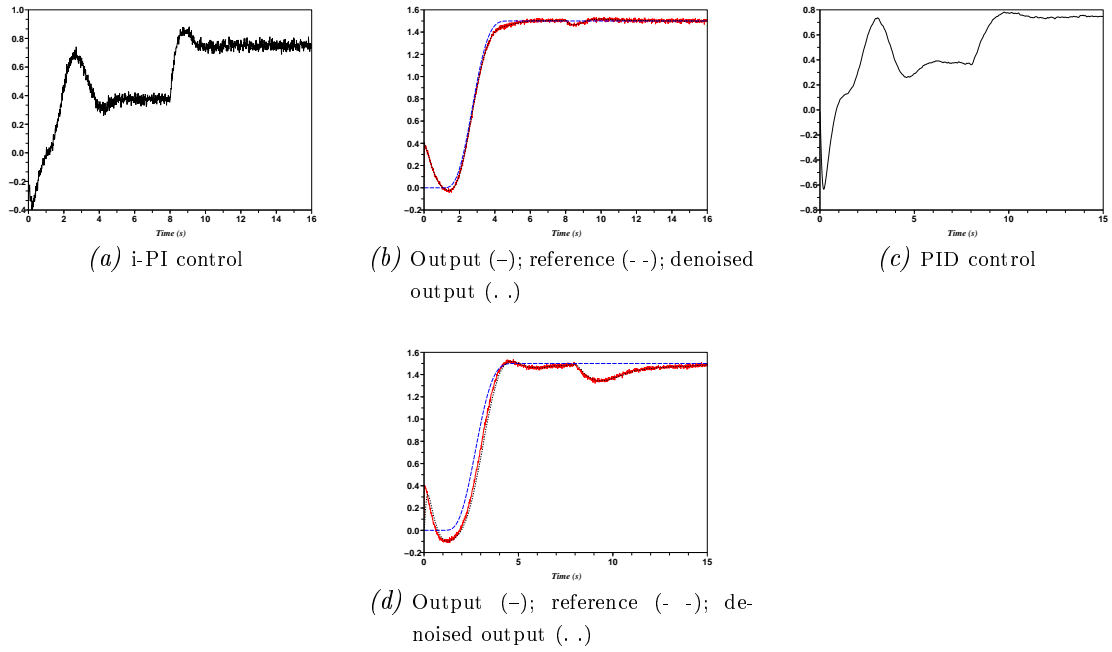


Figure 3. Stable linear monovaryable system, with an actuator's fault

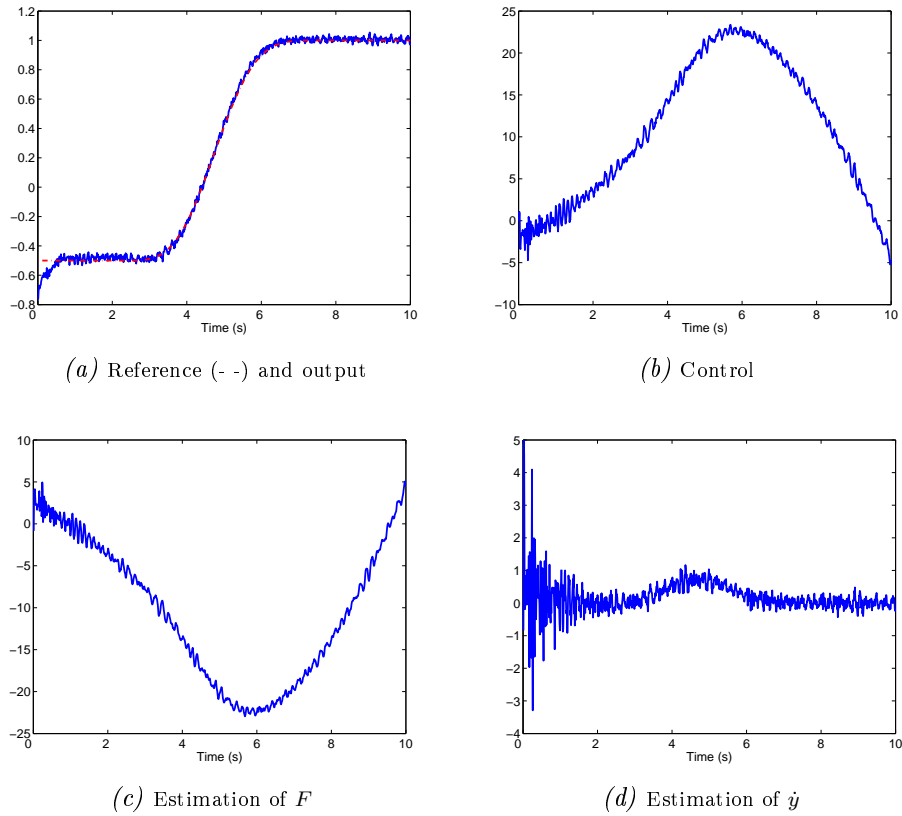


Figure 4. Linear monovaryable system with a large spectrum

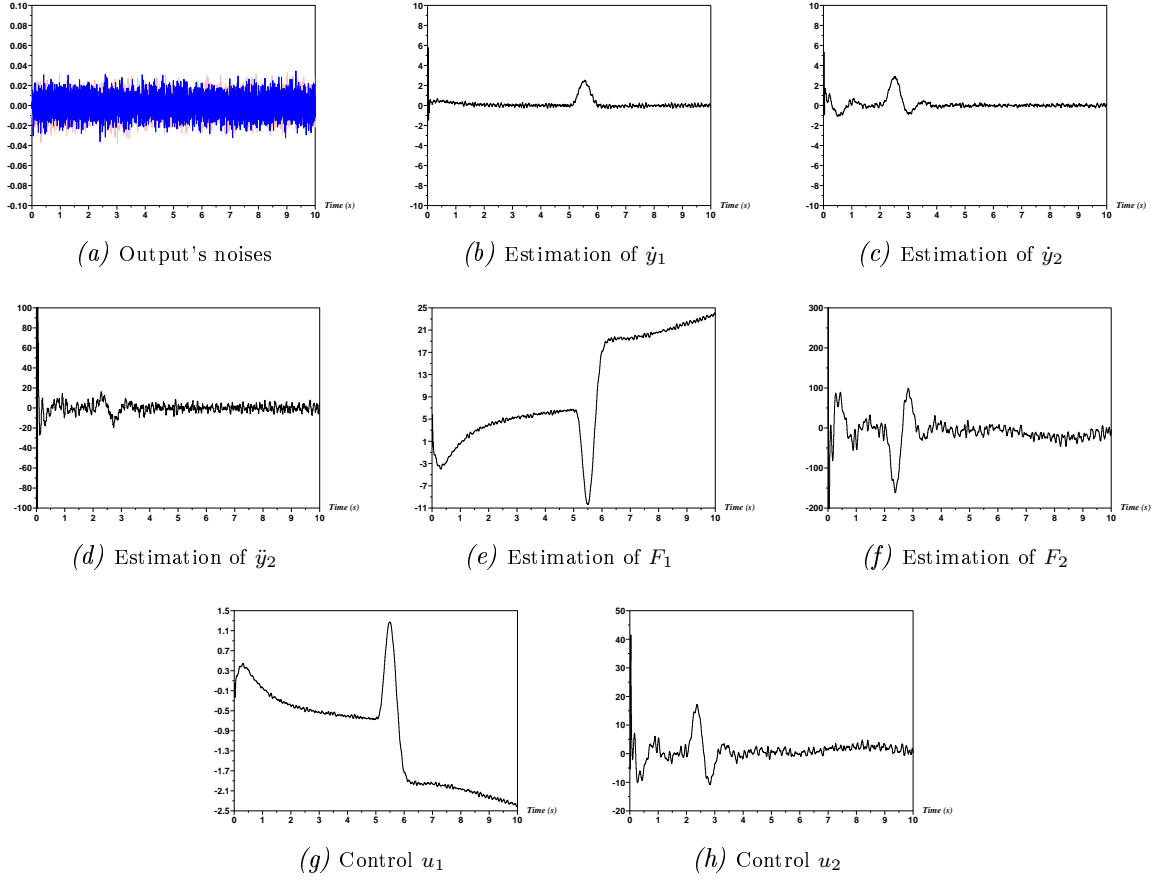


Figure 5. Linear multivariable system

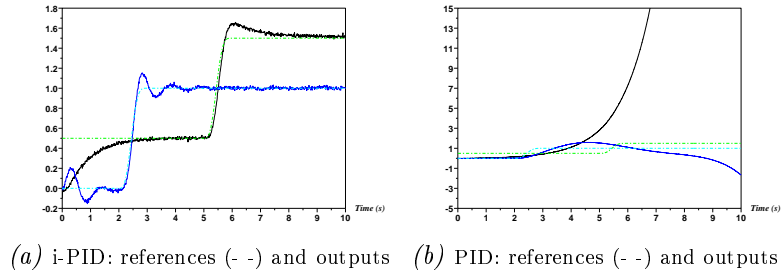


Figure 6. Linear multivariable system

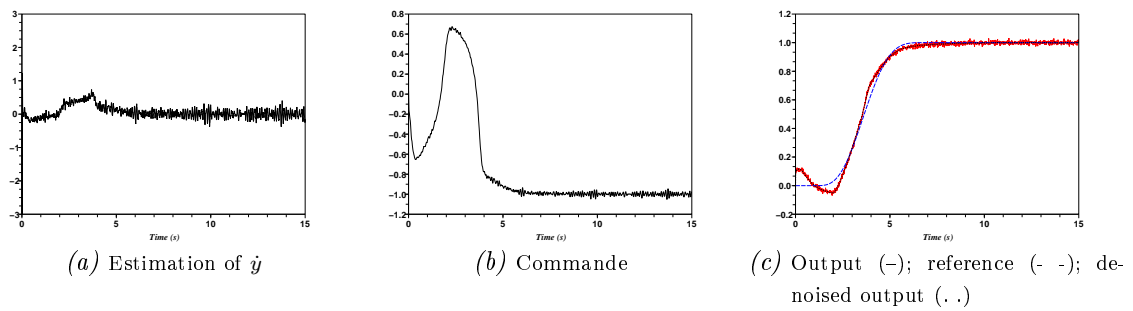


Figure 7. Instable nonlinear monovariale system

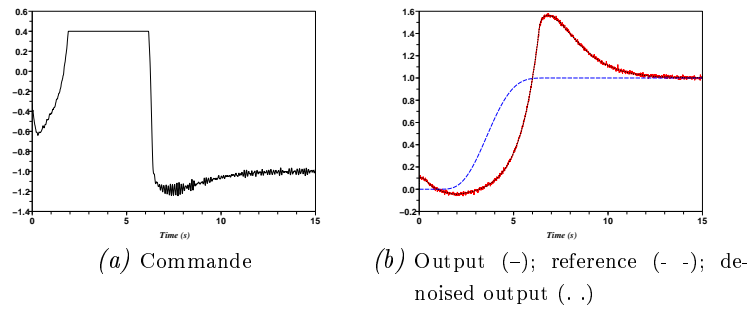


Figure 8. Instable nonlinear system: saturated control without anti-windup

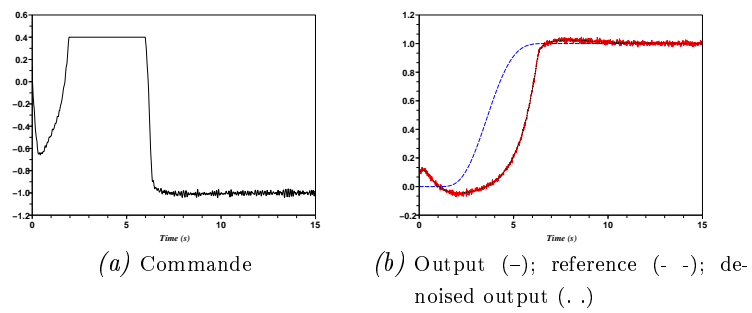


Figure 9. Instable nonlinear system: saturated control with anti-windup

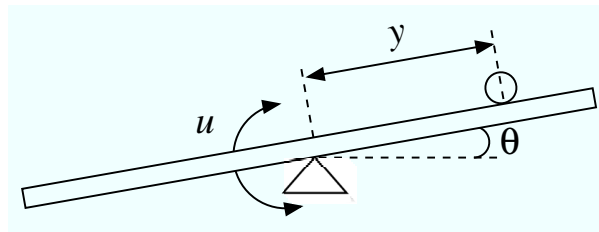


Figure 10. The ball and beam example

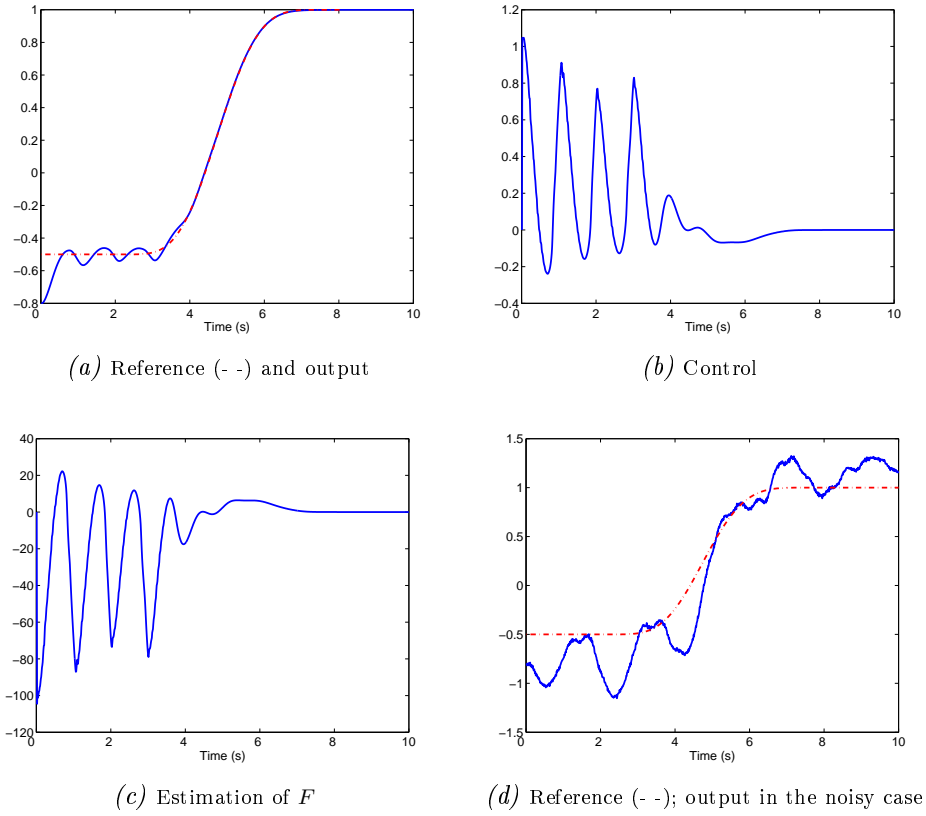


Figure 11. Polynomial trajectory for the ball and beam

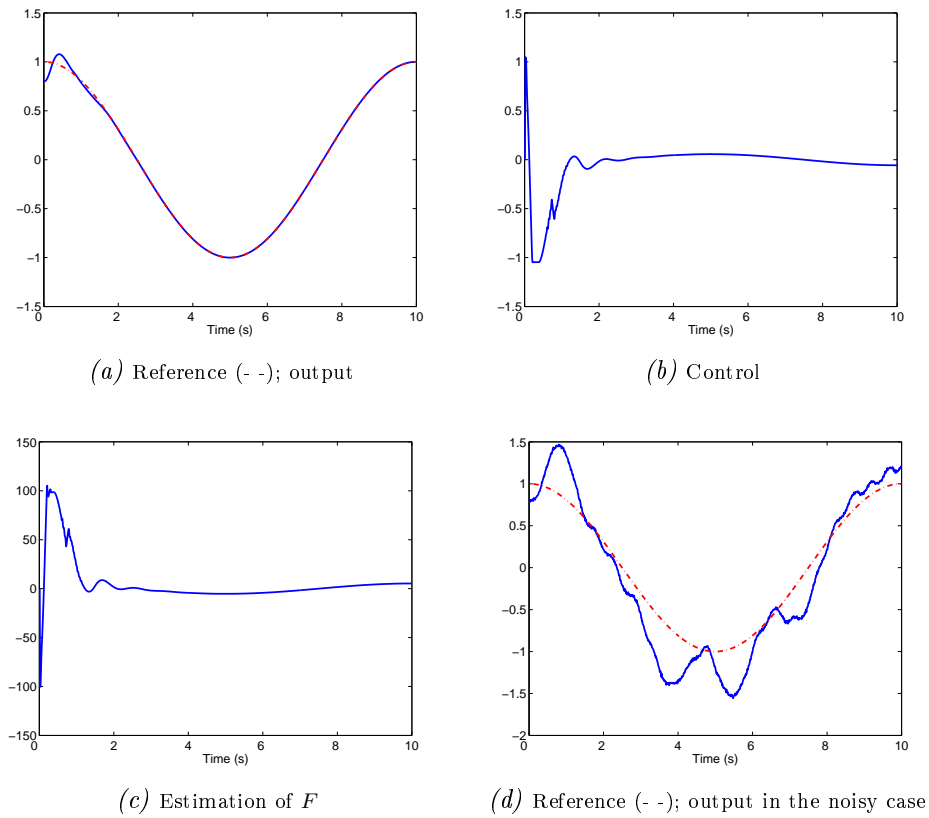


Figure 12. Sinusoidal trajectory for the ball and beam

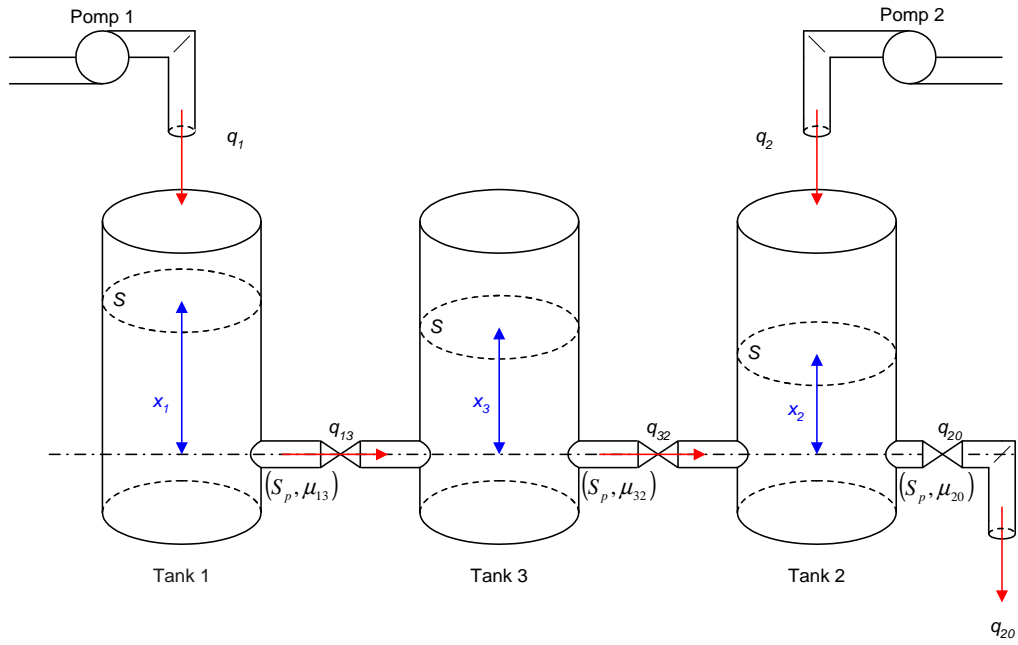


Figure 13. The 3 tank system

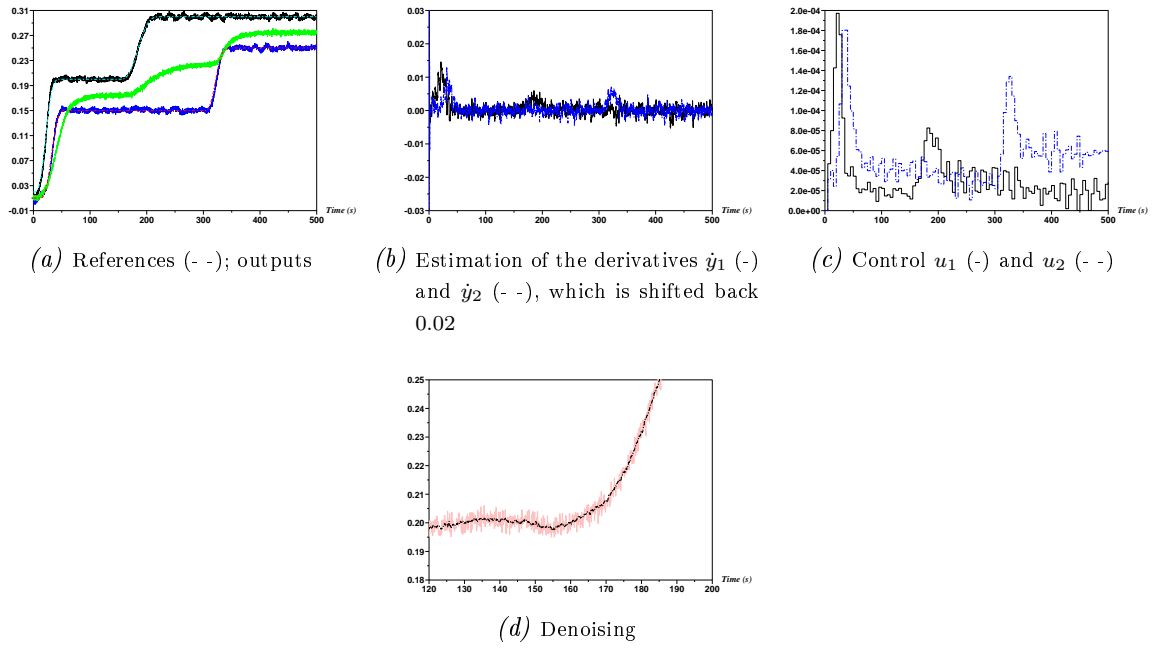


Figure 14. Simulations for the 3 tank system

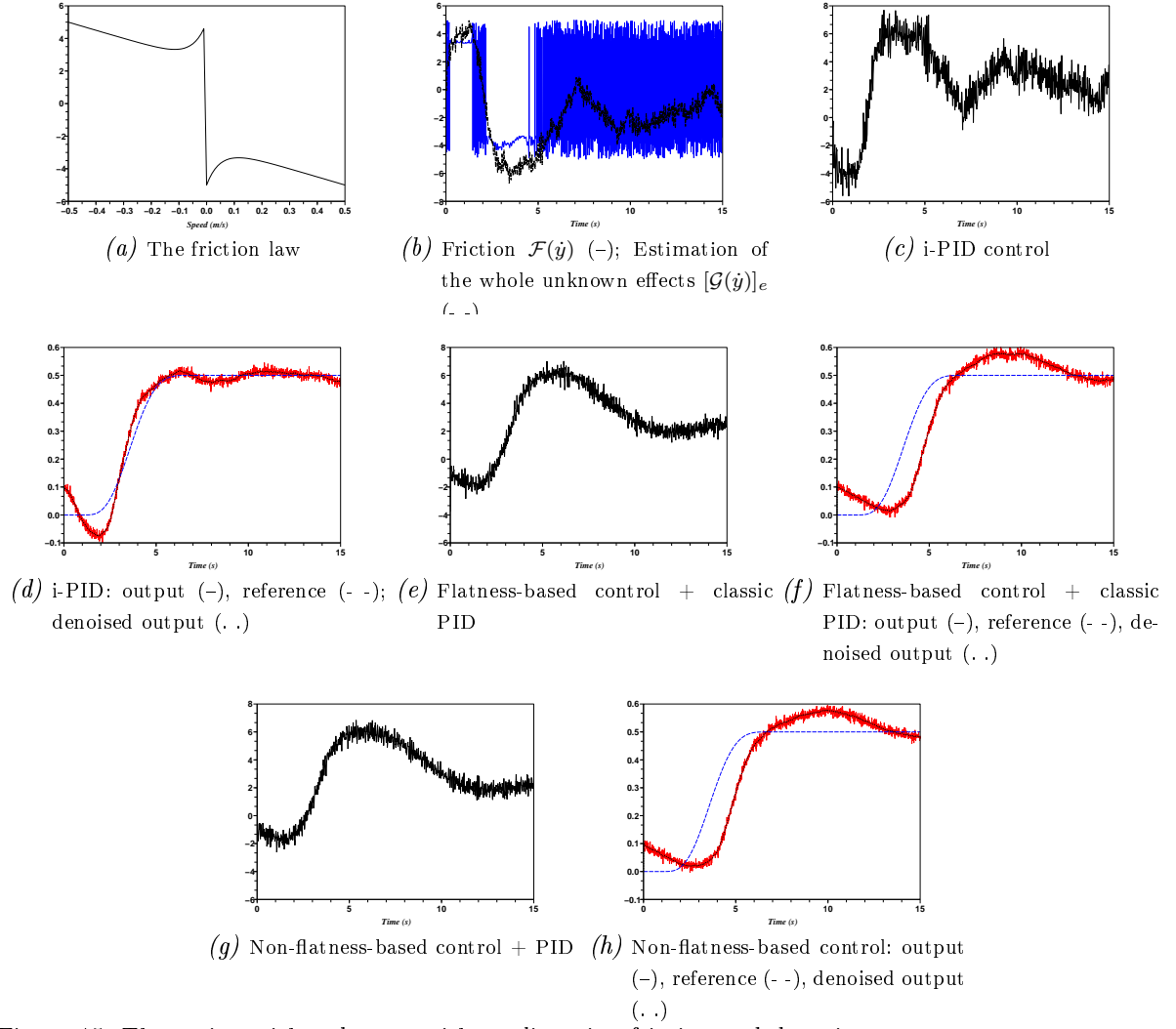


Figure 15. The spring with unknown with nonlinearity, friction and damping

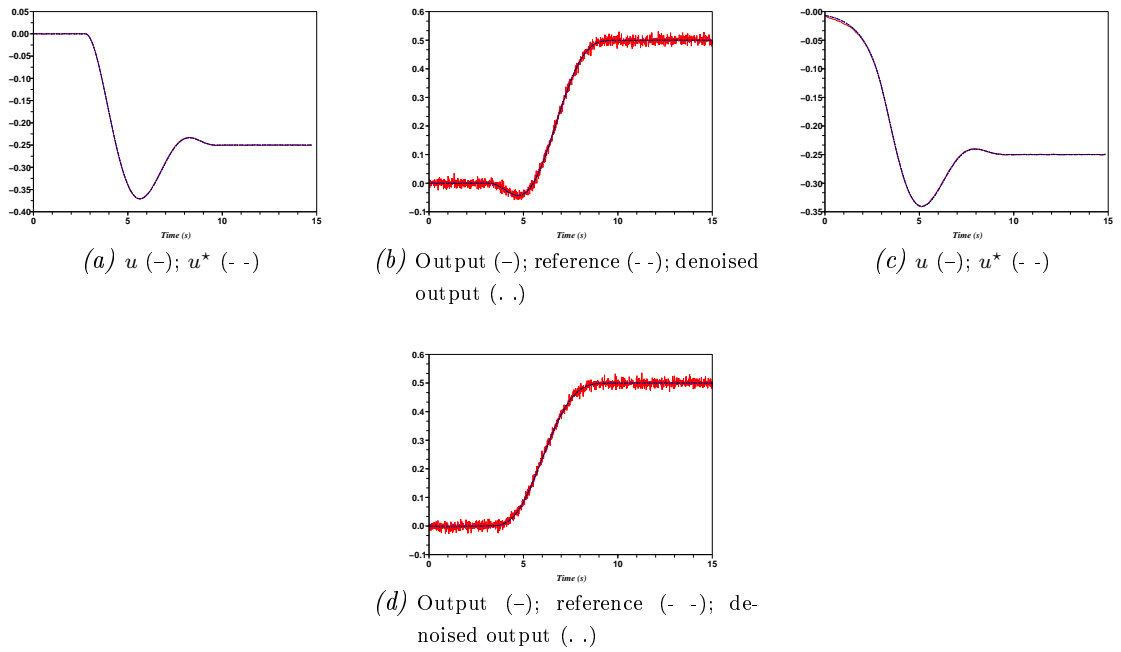


Figure 16. Non-minimum phase system

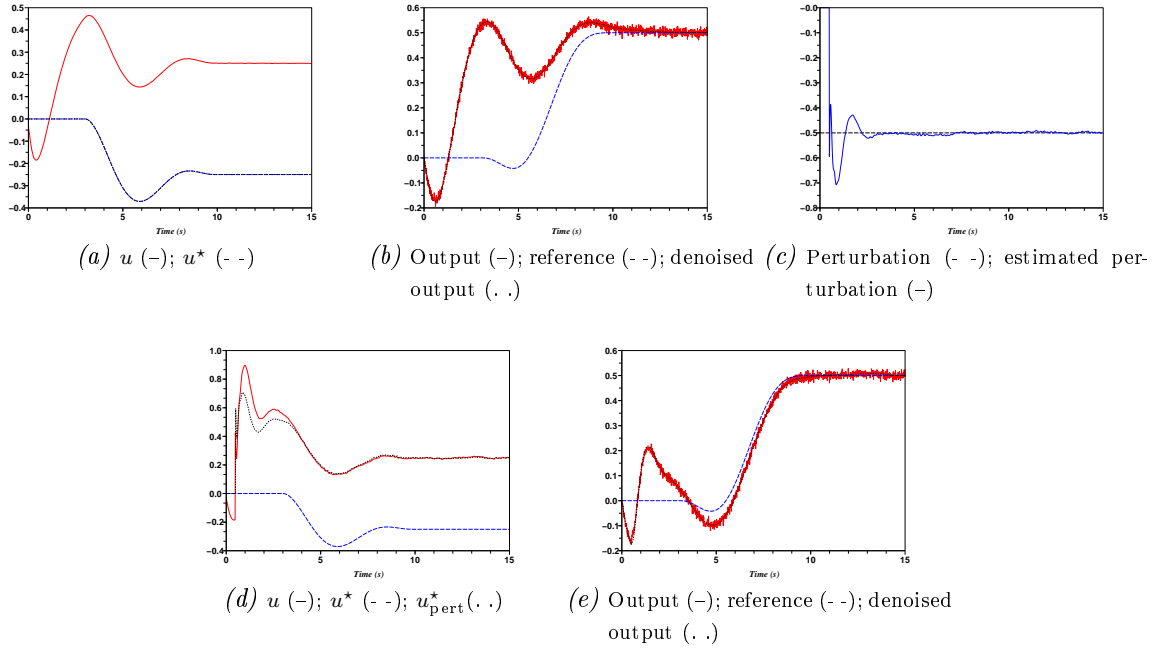


Figure 17. The non-minimum phase system where the first effect is not modeled

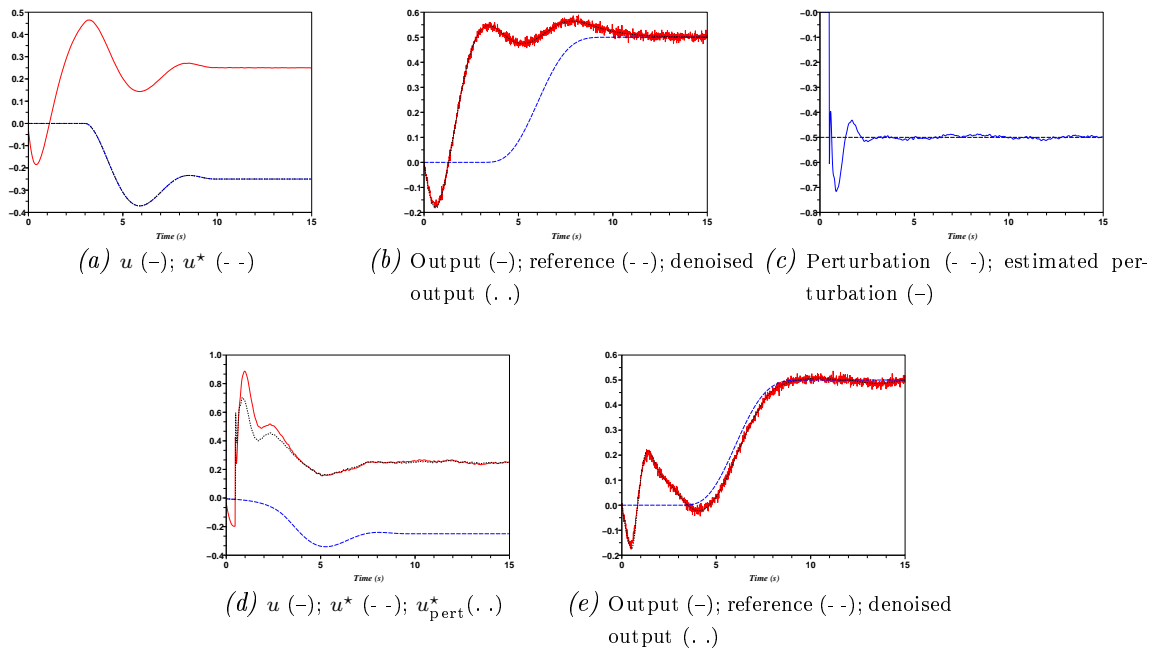


Figure 18. The non-minimum phase system where the first effect is not modeled

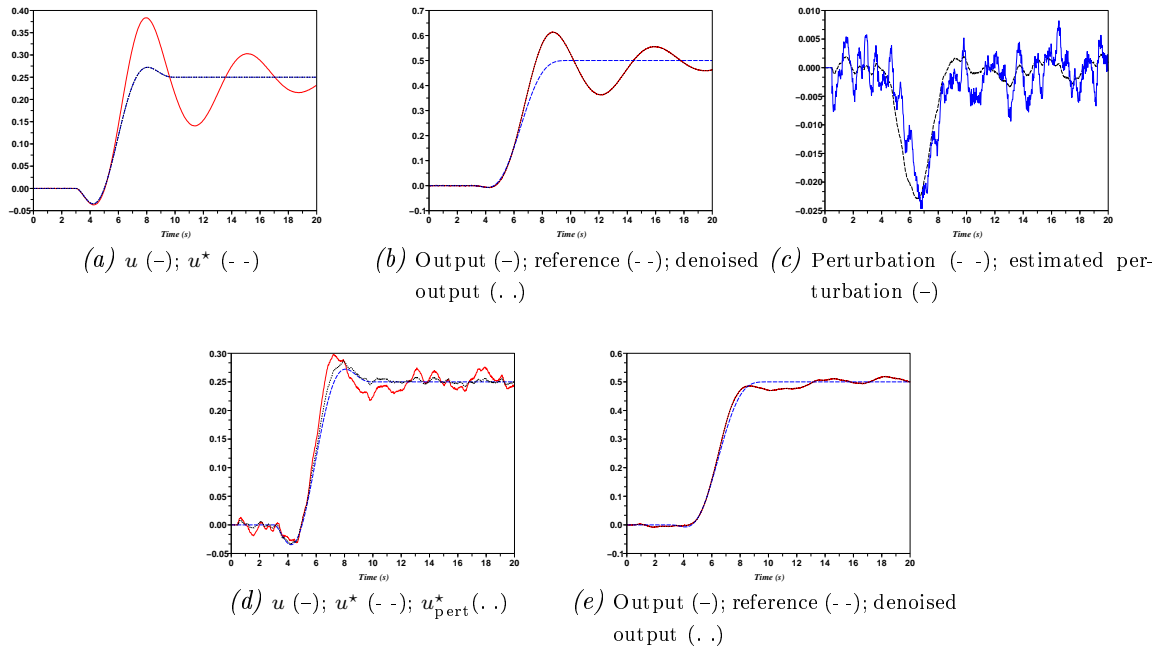


Figure 19. The non-minimum phase system where the second effect is not modeled