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Artificial Intelligence Application for Crude Distillation Unit: An overview

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Abstract. Artificial intelligence (AI) with its efficiency for complex systems is growing in popularity in many engineering fields. The ability of an AI method to be successfully applied is highly dependent on the previous research, which makes knowledge sharing within and across fields extremely valuable. This work focuses on crude distillations units (CDU), whose energy optimization has been a tremendous challenge because of its complexity. The presented overview shows that soft sensors are the most common application of artificial intelligence for a CDU, although a number of recent publications focus on optimization problems. The approaches for optimization are very diverse, which makes them hardly applicable in the current engineering practice. This work provides a guideline for selecting the right method, but also addresses the fact that different methods excel at different problems and with different data set sizes. For neural networks (NN), this further depends on their architecture and hyperparameter adjustment. This urges future research, whose goal could be a workflow that would automatically adapt methods and perform parameter tuning with minimum user input.

Keywords: Crude Distillation Unit (CDU), Artificial Intelligence (AI), Machine Learning (ML), Neural Network (NN), Sustainability.

1 Introduction

Artificial intelligence is a dynamically developed field, whose significance grew within various industries over the last few decades. While the origins of artificial intelligence (AI) and early neural networks (NN) can be traced 1940s [1], the breakthrough did not happen until the new millennium when rapid hardware development allowed for practical implementation [2].

Nowadays, AI has some extent of successful implementation in virtually all aspects of everyday life, including engineering. Some highly-cited published engineering applications range from optimization of constrained design problems [3], through multiagent and holonic manufacturing systems [4], risk analysis and maintenance [5], to water quality prediction [6].

Some of the important engineering challenges to address using artificial intelligence are the reduction of energy consumption and related emissions, as well as sustainability of processes in general. Whereas a Scopus search "TITLE-ABS-KEY (artificial AND intelligence) OR TITLE-ABS-KEY (machine AND learning) OR TITLE-ABS-KEY (neural AND network)" returns almost 1.2 million results, mere 3,400 documents mention "sustainability" in their title, abstract or keywords.

One of the industries where the abovementioned sustainability-related keywords are relevant is petroleum refining, whose global primary energy consumption is estimated to be over 5 % [7]. Within oil refineries, the key equipment which is also related to the highest energy consumption is crude distillation unit (CDU), which might use around one-third of the refinery primary energy demands [8].

Chemical engineering, including oil refining, somewhat lagged behind the general increasing trend in artificial intelligence implementation at the beginning of the millennium. This is demonstrated in Fig. 1. However, the last couple of years showed an unprecedented growth, from around 200 publications indexed in Scopus per year between 2015 and 2017 to 700 records in 2020.

Fig. 1. All results for the "artificial intelligence" Scopus search compared to the same search narrowed down to the subject areas "Chemical Engineering".

This work presents an overview of artificial intelligence applications for the CDU over the last decade, which, especially in its second half, recorded such a rapid increase in publishing activity within chemical engineering. However, only a limited number of publications deal with the energy intensity of the process, as will be shown below. The following chapters present the CDU process (2), literature search methodology (3) and the main findings in the literature (4).

2 Process description

A crude distillation unit (CDU) represents an essential separation step and the first of the fundamental unit operations in any petroleum refinery. Its main purpose is to separate the crude oil feed, a mixture of hydrocarbons with a wide range of boiling points, into semi-finished or final products based on their respective volatility. A common process layout of such a unit is shown in Fig. 2.

Fig. 2. A simplified process diagram of a typical crude distillation unit; adapted from [17].

Before entering the *atmospheric distillation column* (Fig. 2), the crude oil feed is preheated in a heat exchanger network or series of networks called *preheat trains* (Fig. 2). Heat is recovered from relatively hot streams elsewhere in the process. This heat integration allows for a higher energy efficiency of the unit.

The remainder of the required heat input is provided in a *furnace* (Fig. 2), at the outlet of which the crude oil is partially vaporized and enters the flash zone of the *column*. A relatively steep temperature gradient exists within the *column*, with the lowest temperature at the top. The gradient is caused and controlled by the overhead *condenser* (Fig. 2) as well as *pump-around cooling* (Fig. 2) along the column. The temperature at a specific point in the column is dependent on the vapor-liquid contact between the internal reflux stream and vapor flowing up from the flash zone. The temperature profile determines the position of side draws where different products can be extracted from the main *column*.

Side strippers (Fig. 2) are used to remove light ends (light hydrocarbons) from the products. This is necessary to adjust products' distillation curves and other properties according to the specification. Stripping is done by *stripping steam* (Fig. 2) injection, which is also used at the bottom of the main column, or via a reboiler.

The heaviest fraction, *atmospheric residue* (Fig. 2), leaves at the bottom of the column and is further processed in vacuum distillation and/or other processes. The number and character of lighter liquid products from the side strippers and condenser may vary, but these are commonly (from heaviest to lightest) *gas oil, kerosene, heavy naphtha,* and *light naphtha* (Fig. 2). The light ends and other non-condensable gases are separated in the *condenser* (this stream is omitted in Fig. 2 for simplicity).

Even the significantly simplified illustration and description of the unit demonstrates the high complexity of the system. This work's authors have recently dealt with a CDU system in a similar scope but in a high level of detail. The number of manipulated variables in this case study, already narrowed according to energy optimization purposes, was close to 50. The number of all variables, including dependent and nonrelevant variables, easily goes into hundreds for a typical CDU.

From the authors' experience, even conventional process simulation as the most popular method to design, optimize and troubleshoot crude distillation units can fail to obtain results, given an inadequate combination of manipulated variables. While this is not the method's drawback and often simply indicates an infeasible operating point, it calls for application of unconventional and progressive methods, effective for highdimensional data and complex problems. For this reason, the following chapters explore the existing applications of artificial intelligence to CDU.

3 Literature search methodology

The goal of the methodology is to find relevant records, in which artificial intelligence (AI) is applied to a crude distillation unit (CDU) regardless of the specific purpose. To perform such search, four keyword phrases are used:

- ─ crude distillation (the investigated process), AND
- ─ artificial intelligence (as the most general term), OR
- ─ machine learning (the largest subcategory of AI), OR
- ─ neural network (the most pronounced method of AI),

The abstract and citation database Scopus is used for the search. The phrases above are looked for within titles, abstracts and keywords. Also, the year range is limited to 2011–2021. The initial search is narrowed by excluding the results which could not be retrieved (reason A), are not available in English (reason B), are not related to crude distillation or artificial intelligence (reason C), are not individual contributions (e.g., conference reviews; reason D), or use the same method or have the same purpose as in the authors' previous work (reason E).

Within the final literature set included in the overview, four main data items are collected wherever available:

- ─ used AI and non-AI methods,
- ─ purpose of the work,
- ─ size and/or division of a data set into training, test and validation sets if applicable,
- ─ affinity to the topics of sustainability, energy and emissions.

The described multi-step procedure will lead to a relevant set of documents that can be analyzed with respect to qualitative and quantitative parameters that allow for discussion, recognition of well-covered aspects of the process and identification of potential future directions that are not as well-developed.

The main goal, however, is to provide an insight to engineers and researchers dealing with the same tasks that can already be found in the literature. Instead of "reinventing" the wheel", they can rely on the methods that have already been created and established.

4 Main findings in the literature

The initial search resulted in a group of 45 records. Three following checks, which can be described as a) availability (exclusion reasons A and B), b) eligibility (exclusion reasons C and D), c) uniqueness (exclusion reason E), resulted in a final set of 16 documents that were thoroughly examined and included in the final overview. See Fig. 3 for details about how many documents were excluded in each step.

Fig. 3. Step-by-step selection of the final literature set from the initial search.

4.1 Categorization

Based on their purpose, the 16 items can be divided into the following categories:

- 1. Control of the CDU (Table 1)
	- a. Soft sensors 6 records;
	- b. Predictive control 1 record;
- 2. Optimization of the CDU (Table 2)
	- a. Heat, energy and/or exergy budget 4 records;
	- b. Cost 2 records (1 design, 1 operation);
	- c. Non-specific opt. (1 record);
- 3. Other (Table 3)
	- a. Property estimation 1 record;
	- b. Risk management 1 record.

The results of the investigation in Tables 1–3 show what methods the authors used, the purpose of their efforts, a condensed description of their work, the size and distribution of their data set, and links to the topics of energy, emissions or sustainability (EES).

The application for soft sensors is prevalent, mostly for quantities that cannot be measured continuously, or where the related analysis is time- or cost-intensive (cut point temperature, dry point, vapour pressure).

Methods	Purpose	Description	Training/ Test/ Validation	EES Ref.	
1a. Soft sensors					
-K-means -K-nearest neighbors (K- NN) -Random forest (RFc) -Support Vector Classifi- cation (SVC) -multilayer perceptron (MLP)	soft sensor for the "nee- dle penetra- tion" analy- sis (UNE- EN 1426:2015)	-GridSearch used to op- timize hyper parameters for each method (e.g. number of neurons in 1 hidden layer of the MLP) -94 inputs -1 output -K-means best for this application	90 % / 10 % (268) samples)	No	[9]
-multiple linear regres- sion (MLR) -linear neural network (LNN) -multilayer perceptron (MLP) -radial basis function (RBF)	prediction of Reid vapor pressure (RVP) of the light naph- tha product	-96 data samples -number of neurons and 25 % / algorithms 25 % learning tested to find the best- performing combination -MLP $(6-4-1)$ and RBF $(6-7-1)$ best results	50 % $/$	No	$[10]$
-deep belief network (DBN) -restricted Boltzmann ma- chines (RBM)	soft sensor (ASTM 95% cut point temperature)	-DBN consists of a se- 251/100 ries of RBMs -16 inputs -1 output -architecture $16/20/16/1$ -compared and superior to SVM, PLS, NNPLS		No	[11]
-multilayer perceptron (MLP) -least absolute shrinkage and selection operator (LASSO)	soft sensor for the esti- mation of the kerosene D ₉₅	-compared to sequential 240 / 121 backward multiplayer perceptron (SBS-MLP), normalized mutual in- formation feature selection (NMIFS) and ELM (Elman network) -25 variables -25-4-1 architecture		No	$[12]$

Table 1. Overview of the records related to the process control.

			Training/		
Methods	Purpose	Description	Test/	EES Ref.	
			Validation		
a number of statistical	soft sensor	-the process simulator	$225(50)$ /	Yes	$[13]$
learning methods (partial	(95% cut)	PRO/II to generate data	75		
least squares, neural net-	point tem-	-relevance vector ma-			
works, relevance vector	perature)	chine (RVM) was the			
machine, Bayesian linear		best for this application			
regression, ridge regres-		accuracy, (high >10			
sion)		times faster than NN,			
		high generalization ca-			
		pacity)			
-bootstrap aggregated	estimation	-16 inputs (selected out 200/70/		No	[14]
neural networks (BANN)	of kerosene	of 50	87		
-bootstrap aggregated	dry point	-Aspen HYSYS to gen-			
partial least squares	with varying	erate simulated data.			
(BAPLS)	crudes	random noise added to			
		the data			
		-intentionally limited			
		data set to represent lim-			
		ited dry point analyses			
		-BANN for oil classifi-			
		cation, BAPLS (partial			
		least square) for the dry			
		point prediction			
1b. Predictive control					
- feedforward NN (FNN)	model pre-	-CVXOPT (quadratic	1500	No	$[15]$
-stochastic optimization	dictive con-	solver programming	epochs		
algorithm Adam (train-	trol for a	used for data generation			
ing)	CDU	and as a benchmark)			
		-architecture: 1072			
		$(1664 - 1920) \times 3$ hidden			
		layers / 32			
		-NN milliseconds, QP			
		solver tens of seconds,			
		negligible performance			
		loss			

Table 1 Continued. Overview of the records related to the process control.

The optimization purposes are almost as common as soft sensors and very often focus on or at least account for energy demands. However, the variety of used approaches make it uneasy to select the right methods for engineering applications. Authors often claim their approach is superior to others, and rightfully so – for the given problem, data set size, selected network architecture and hyperparameters.

Methods	Purpose	Description	Training/ Test/ Validation	EES Ref.	
2a. Heat, energy and/or exergy budget optimization					
-neural network (NN) -Taguchi method -genetic algorithm (GA)	optimize cut point tem- peratures and specific energy, deal with feed uncertainty	- ANN predicts prod- ucts' cut points based on feed the composition (reduces) calculation time) - 3 hidden layers (13, 17, 16 neurons) - Aspen HYSYS used for energy demands cal- culation - Taguchi and GA opti- mize cut point tempera- tures	85 % / 15 % (192 data) points)	Yes	[16]
-feedforward NN (FNN) -simulated annealing (SA)	retrofit of heat ex- changer net- work (HEN) for optimiz- ing CDU op- eration	-1 hidden layer -scenarios generated in Aspen HYSYS -profit is the objective function to maximize	70% / 15 % / 15 % (800 data) points)	Yes	[17]
-bootstrap aggregated neural networks (BANN)	maximiza- tion of ex- ergy effi- ciency of a CDU	-BANN contains 30 NNs -Aspen HYSYS used for operating data genera- tion	50% / 30% / 20 %	Yes	$[18]$
-evolutionary algorithm assisted by adaptive surro- gate functions (EASF) -radial basis function (RBF) -approximation error fuzzy control strategy (AEFCS)	maximize distillation heat supply from reflux streams	-Aspen Plus – rigorous N/A model -DEA (differential EA) - optimization -RBF surrogate model, three layers $-AEFCS$ – model man- agement -ba		Yes	[19]

Table 2. Overview of the records related to process optimization.

Methods	Purpose	Description	Training/ Test / Validation		EES Ref.		
2b. Cost optimization							
-neural network (NN) -support vector machine (SVM) -genetic algorithm (GA)	design of a crude distil- lation unit with opti- mized cost	-Aspen HYSYS used to build a surrogate model (ANN) while feasibility constraints are gener- ated using a SVM to op- timize the column con- figuration -annual cost as an objec- tive function -18 inputs -46 output (divided into multiple NNs) -one hidden layer (10 neurons)	-70% / 15 % / 15 % (NN) $-75%$ 25 % (SVM)	Yes	$[20]$		
-wavelet neural network economic (WNN) -line-up competition algo- rithm (LCA)	optimization of a CDU under pre- scribed con- straints	-WNN predicts the CDU behavior, LCA ap- plied to the constrained optimization problem hidden -one layer, 30 neurons -Aspen Plus used for the rigorous model -WNN superior to RBFNN and BPNN. LCA superior to GA and PSO	350/150	Yes	$\lceil 21 \rceil$		
2c. Non-specific optimization							
efficient dropout neural network (EDN)	optimization problem of crude oil distillation units	-advantageous for high- dimensional multi-ob- jective expensive opti- mization problem -up to 100 decision vari- ables and 20 objectives -two hidden layers -sensitivity analysis on parameters	various	No	[22]		

Table 2 Continued. Overview of the records related to process optimization.

In a sense, both implementations from the Other category (Table 3) can be understood as soft sensors, because both TBP data [10] and corrosion rate [12] are quantities that are costly to measure and not available in real time. They are excluded from the first category because of the limited relation to the process unit and the lack of a tangible location where the soft sensor would predict the quantities.

Methods 3a. Property Estimation	Purpose	Description	Training $/$ Test / Validation	EES Ref.	
sure independence screening and sparsifying operator (SISSO)	ML used for the creation of a simple equation (TBP data to products' relative amounts)	laboratory distillation of $-$ crude oil		No	[23]
3b. Risk management					
-feedforward NN (FNN) -multiple linear regres- sion analysis (MLRA)	corrosion prediction and the re- lated risk management	-11 inputs -two hidden layers -3 outputs (pH, chloride salt and content in crude) -MLRA used to predict the corrosion rate	$60 - 90 %$ $40 - 10%$ (24 points)	N ₀	[24]

Table 3. Overview of the other records from the literature search.

4.2 Discussion

Feedforward neural networks (FNN), and multilayer perceptron (MLP) which belongs to this category, were most dominant across all the applications. There was, however, a slight bias introduced to the search since NN were the only AI method that was explicitly searched for.

One common feature is the lack of data, which is often compensated using process simulation (Aspen HYSYS [14,16,17,18,20], Aspen Plus [19,21], PRO/II [13]) to generate a data set mimicking real operating data. While the motivation is sometimes the simplicity of data generation, this might indicate an underlying problem of the industry's conservatism toward artificial intelligence and limited willingness to share data with researchers.

While there were some attempts to optimize the architecture and parameters in the assessed literature [9,10], the trial-and-error approach is still most common for this challenge as well as method selection.

5 Conclusions

Artificial intelligence (AI) has been successfully applied to a number of engineering problems and has hugely grown in popularity in chemical engineering lately. In this work, some recent publications which applied artificial intelligence to the most energyintensive oil refining process, crude distillation, were examined with respect to their purpose, methods, data set character and sustainability ideas.

Based on a multi-step search and selection, 16 records were included in the overview. It was found out that soft or virtual sensors are the most typical implementation of artificial intelligence for this process, while neural networks are the dominant AI method.

The variety of approaches, especially for the optimization of crude distillation units, make AI cumbersome to use for practical engineering problems. An interesting future research direction could focus on the automatic selection of an appropriate algorithm, together with the tuning of hyperparameters associated with machine learning.

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12

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